

010217

GAS CONDENSATES

①

Produced liquid volumes $(\Delta V_o)_i$, sc

Calculate the liquid volume of each component in liquid phase, and add them together.

(C_4, C_5, C_6, C_{7+})

We find the liquid volume (in Gal (US gallons)) by first finding the gas volumes of the components, then convert to liquid volume,

GPM = $\frac{\text{gal (liquid)}}{1000 \text{ scf gas}}$ For every component.

$$C_4: (V_L)_{C_4} = \overbrace{a \cdot (Z_{C_4})_i \cdot (\Delta G_p)_i}^{\text{gas volume}} \cdot \text{GPM}_{C_4}$$

liquid recovery factor
mole fraction
produced wellstream
conversion from gas volume \rightarrow liquid volume.

$$C_5: (V_L)_{C_5} = b \cdot (Z_{C_5})_i \cdot (\Delta G_p)_i \cdot \text{GPM}_{C_5}$$

$$C_6: (V_L)_{C_6} = c \cdot (Z_{C_6})_i \cdot (\Delta G_p)_i \cdot \text{GPM}_{C_6}$$

$$C_{7+}: (V_L)_{C_{7+}} = d \cdot (Z_{C_{7+}})_i \cdot (\Delta G_p)_i \cdot \text{GPM}_{C_{7+}}$$

Total liquid volume $(\Delta V_o)_i$ in Gal.

$$(\Delta V_o)_i = (V_L)_{C_4} + (V_L)_{C_5} + (V_L)_{C_6} + (V_L)_{C_{7+}}$$

in Gal.

Convert to SBL (Barrels) :

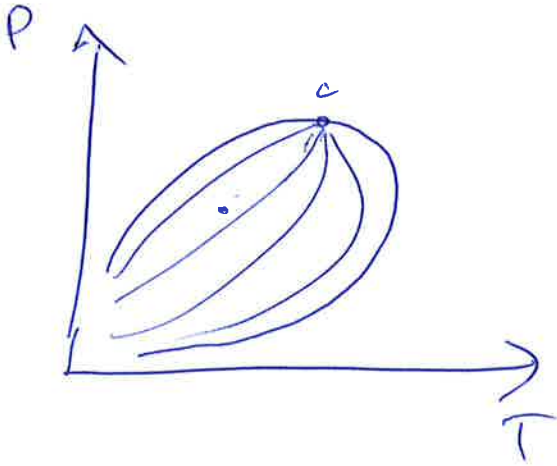
$$1 \text{ bbl} = 42,117 \text{ Gal}$$

⇒ GOR - gas oil ratio - ~~§~~
in pressure interval i

$$GOR_i = \frac{(\Delta V_g)_i}{(\Delta V_o)_i}$$

Initial GOR can be found using
initial reservoir fluid composition.

EQUILIBRIUM CALCULATIONS



Inside two-phase envelope
gas in equilibrium with
oil.

Both composition of oil and
gas, and volumes change
inside the two phase
envelope.

Eq. calculations to determine compositions
and volumes of oil and gas at
given P and T.

Reservoir fluid composition:

$$z_i = \frac{n_i}{\sum n_j}$$

$$w_i = \frac{w_i}{\sum w_j}$$

$$\sum z_i = 1$$

$$\sum w_i = 1$$

Flash calculations:

V mol fraction of gas
L mol fraction of liquid

can determine composition
of oil and gas
phase.

K -values are physical equilibrium constants determining the ratio of mole fraction comp i in gas phase over mole fraction of comp i in liquid phase.

Defined by Dalton's law for ideal gases and by Raoult's law for ideal liquids.

The reservoir fluid is in the two-phase area, at given P and T :

For ideal gas:

$$P = \sum P_i \quad ; \quad P_i = y_i \cdot P$$

Dalton's law

P = total pressure of the gas

P_i = partial pressure of comp i in the gas mixture

y_i = mol fraction of comp i in the gas

For an ideal liquid:

$$P_i = x_i \cdot P_{vi}$$

P_i = Partial vapor pressure for a component i in the liquid.

x_i = mole fraction of comp. i in the liquid.

P_{vi} = vapor pressure of pure component in liquid

* Two-phase area at given P and T:
gas and oil are in equilibrium

$$P_i(\text{gas}) = P_i(\text{liquid})$$

$$y_i \cdot P = x_i \cdot P_{vi}$$

$$\Downarrow$$

$K_i = \frac{y_i}{x_i} = \frac{P_{vi}}{P}$
--

K_i - K-values.

* Ratio of mol fraction comp i in ~~the~~ gas phase over liquid phase.

\Rightarrow K_i can be found in handbooks
in PVT-simulations.

specific for each component at
specified P and T.

Flash calculations

A flash process is also called \rightarrow
 "constant mass expansion" - CME-process

CME: A certain amount of \Rightarrow fluid expands and two are formed, oil and gas.

Increase volume, pressure drops below the P_d , liquid is formed.

For \Rightarrow given P and T in two-phase area. Basis: 1 mole feed or 1 mole initial reservoir fluid.

$$1) \quad V + L = 1$$

$$2) \quad z_i = x_i L + y_i V$$

$$3) \quad K_i = \frac{y_i}{x_i}$$

$$4) \quad \sum x_i = \sum y_i = \sum z_i = 1$$

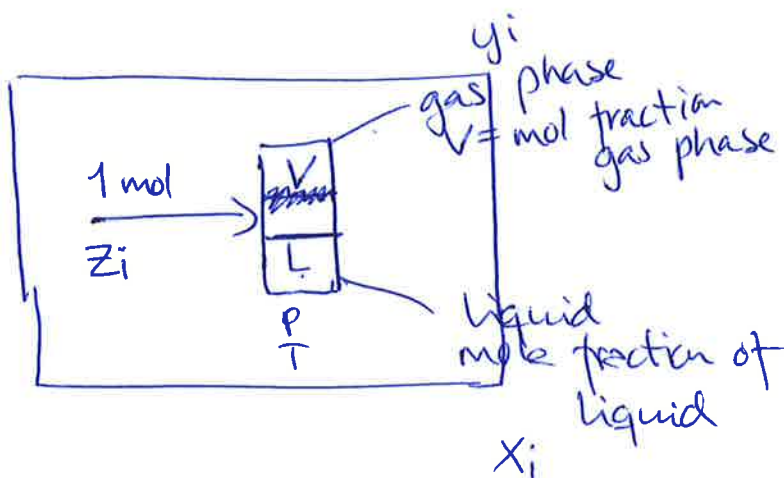
V = mole fraction gas

L = mole fraction liquid

z_i = mole fraction of comp. i in reservoir fluid

x_i = mol fraction of comp. i in liquid phase

y_i = mol fraction of comp. i in gas phase



Combine 2) and 3)

From 3) $y_i = K_i x_i$ and $x_i = \frac{y_i}{K_i}$

Inserted in 2): $y_i = K_i x_i$

$$z_i = x_i L + K_i x_i V$$

$$z_i = x_i (L + K_i V)$$

$$x_i = \frac{z_i}{L + K_i V}$$

y_i : $x_i = \frac{y_i}{K_i}$

$$z_i = \frac{y_i}{K_i} L + y_i V$$

$$z_i = y_i \left(\frac{L}{K_i} + V \right)$$

$$y_i = \frac{z_i}{\left(\frac{L}{K_i} + V \right)}$$

Inserted in 4):

$$5) \sum x_i = \sum \frac{z_i}{L + K_i V} = 1$$

$$6) \sum y_i = \sum \frac{z_i}{\left(\frac{L}{K_i} + V \right)} = 1$$

FLASH
EQUATIONS

Solving flash equations

Solve by iteration - "proving or failing"

Take one of the flash equations:

Pick a value for L , the $V = 1 - L$
Correct L and V values found should summarize to 1.

Newton-Raphson method to be used
Find L and V so that

$$\begin{aligned}L + V &= 1 \\ \sum x_i &= 1 \\ \sum y_i &= 1\end{aligned}$$

Newton-Raphson method

Flash eq. (5)

$$\sum x_i = \sum \frac{z_i}{L + K_i V} = 1$$

Make a function out of it; F

$$F = \sum \frac{z_i}{L + K_i V} - 1 = 0$$

$$F(L) = \sum \frac{z_i}{L + K_i V} - 1 = 0$$

The derivative $F'(L)$:

$$F'(L) = \frac{dF}{dL} = \sum \frac{(K_i - 1) z_i}{[L + K_i (1 - L)]^2}$$

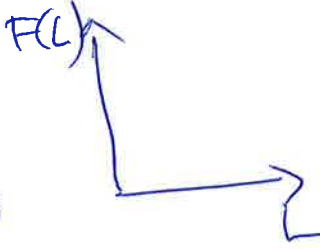
$$\begin{aligned}f(x) &= \frac{u(x)}{v(x)} \\ f'(x) &= \frac{u'(x)v(x) - v'(x)u(x)}{(v(x))^2}\end{aligned}$$

To find correct L and V , procedure:

1) Find correct K_i -values at given P and T , for each component. Z_i is known, from handbooks...

2) Assume a value for L $0 < L < 1$. L_1
($V = 1 - L$)

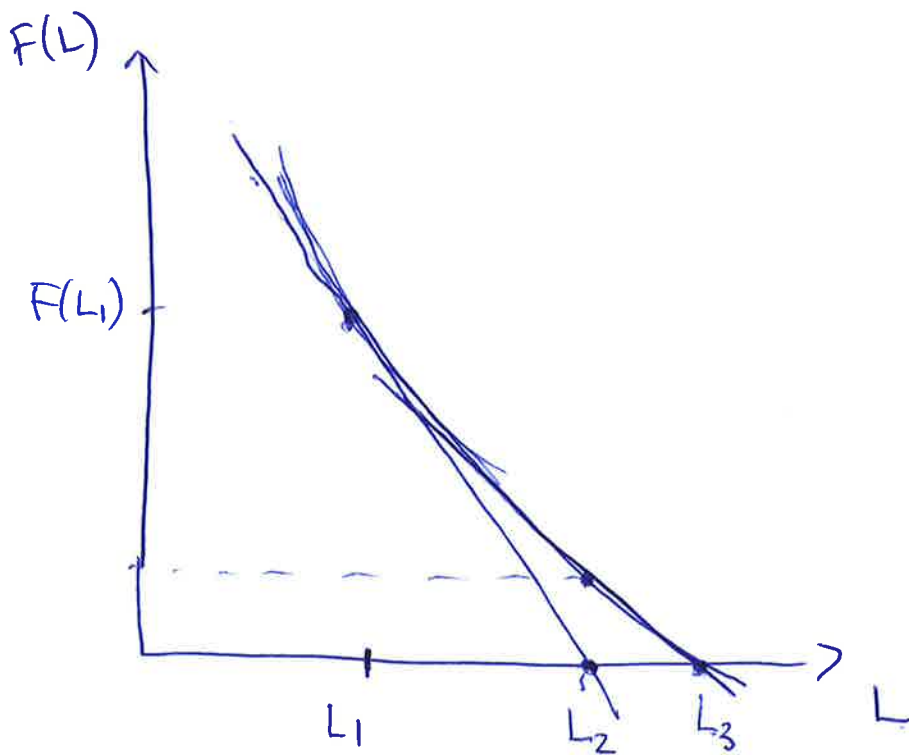
3) Insert L_1 into $F(L)$ and $F'(L)$
calculate $F(L)$ and $F'(L)$.

4) To have a point on a curve $F(L)$
 $(L_1, F(L_1)), F'(L_1)$
↳ slope of tangent 

5) Find new L_2 at $F(L) = 0$

6) Use new L_2 as new value for L

7) Repeat until $F(L) = 0$



$F(L_3) \approx 0$, Then L_3 is correct mole fraction liquid, $V \approx 1 - L_3$

Insert correct values of L and V into flash equations.

Can calculate compositions of oil and gas:

$$\text{oil: } \sum x_i = \sum \frac{z_i}{L + K_i V} = 1$$

$$\text{gas: } \sum y_i = \sum \frac{z_i}{\frac{L}{K_i} + V} = 1$$