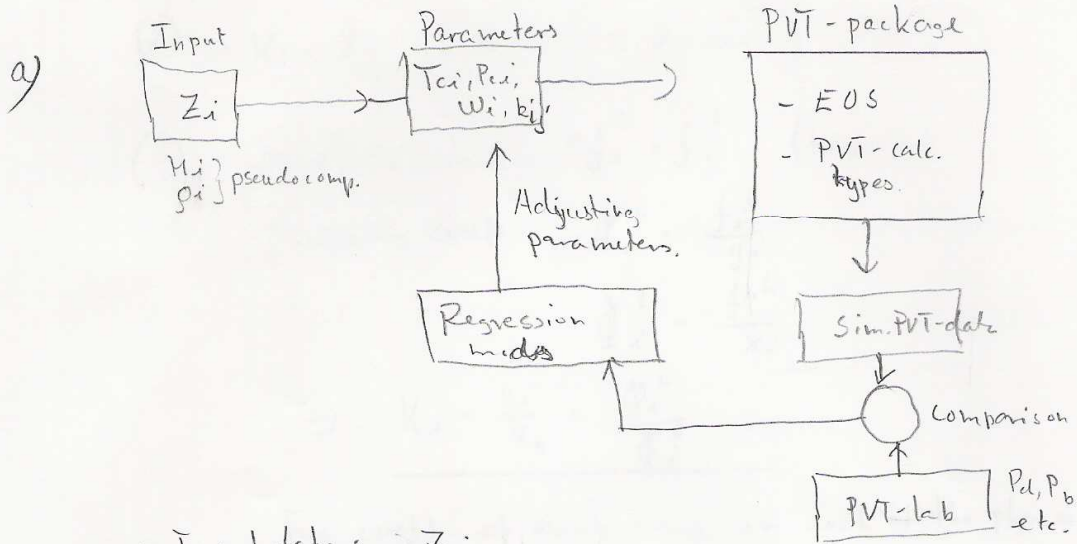


Oppgave 1



- Input data: Z_i

- p_i and M_i for pseudo-comp.

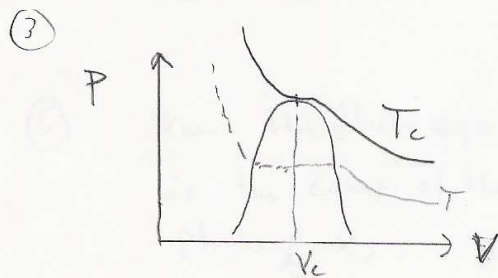
- Parameters: $T_{ci}, P_{ci}, W_i = f(M_i, p_i)$ For pseudo-comp.

//

b)

① $P = P^{rep} - P^{at}$ ↑ P^{rep} : tiltrekningskrefter mellom molekylar
↑ P^{at} : repulsive krefter mellom molekylar

② $a(T)$: beskriver interaksjon mellom molekylar
 b : volumet som molekylene okkuperer.



ved T_c og P_c :

$$\left[\left(\frac{\partial P}{\partial V} \right) = \left(\frac{\partial^2 P}{\partial V^2} \right) = 0 \right]_{T_c, P_c}$$

Hervor 2 ligninger med 2 ukjente

a_i og b_i kan bestemmes.

(2)

c) ① Z_G : compressibility of the vapor phase
 Z_L : " " " liquid "

② $K_i = \frac{y_i}{x_i}$, $K_i = f(T, P, \text{comp.})$

③ At equilibrium: $f_i^G = f_i^L$ (fugacity)

Fugacity coeff. $\Phi_i^G = \frac{f_i^G}{y_i}$

$\Phi_i^L = \frac{f_i^L}{x_i}$

$\Rightarrow K_i = \frac{y_i}{x_i} = \frac{\Phi_i^L}{\Phi_i^G}$

Fug. coeff. of each comp. in each of the phases:

$\ln \Phi_i = - \frac{1}{RT} \int_{\infty}^V \left[\left(\frac{\partial P}{\partial n_i} \right)_{T, V, n_j} - \frac{RT}{V} \right] dV - \ln Z$
↑ compress.

PS: (Forventer ikke at de kan denne formelen)

④ Flash equations. (1 mol fluid)

① $L+V=1$

② $z_i = L \cdot x_i + V \cdot y_i$

③ $K_i = \frac{y_i}{x_i}$

④ $\sum x_i = \sum y_i = \sum z_i = 1$

$\Rightarrow \sum x_i = \sum \frac{z_i}{L + K_i \cdot V} = 1$

~~$y_i = K_i \cdot x_i$~~

Leses ved iteration.

Konvergens $\Rightarrow L$ and V .

⑤ When the flash equation is solved, each term is the comp. of the actual comp. in the liquid phase, x_i .

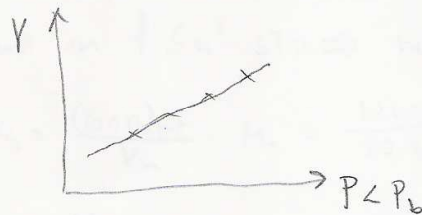
$\Rightarrow y_i = K_i \cdot x_i$ comp. in gas phase.

Oppgave 2.

3

- a) BHS :- because $P_i \gg P_b$
- slow production with $P_{wt} > P_b$.

- b) Plot of Y vs. P should give a straight line.



if P_b is correctly determined.

$$Y = \frac{P_b - P}{P \left(\frac{V_k}{V_n} - 1 \right)} \quad (P < P_b)$$

c)

$$P_i = 450 \text{ bar} \Rightarrow (B_0)_i = 0.9693 \frac{\text{m}^3}{\text{m}^3} \cdot 1.340 \frac{\text{m}^3}{\text{Sm}^3} = 1.2989 \frac{\text{m}^3}{\text{Sm}^3}$$

$$P_b = 253.3 \text{ bar} \Rightarrow (B_0)_b = 1.340 \frac{\text{m}^3}{\text{Sm}^3}$$

$$\text{HCPV} = 10^6 \text{ m}^3 \cdot \Phi(1 - s_{wr}) = 2 \times 10^5 \text{ m}^3$$

$$V_{sto} = \frac{\text{HCPV}}{(B_0)_i} - \frac{\text{HCPV}}{(B_0)_b} = \underline{4.722 \times 10^3 \text{ Sm}^3}$$

$$(\text{GOR})_{tot} = 73.7 + 31.1 + 21.3 = 126.1 \text{ Sm}^3/\text{Sm}^3$$

$$V_g = (\text{GOR})_{tot} \cdot V_{sto} = \underline{5.954 \times 10^5 \text{ Sm}^3}$$

d)

$$(\gamma_g)_{av} = \frac{(\text{GOR})_1 \cdot (\gamma_{g1}) + (\text{GOR})_2 \cdot (\gamma_{g2}) + (\text{GOR})_3 \cdot (\gamma_{g3})}{(\text{GOR})_{tot}}$$

$$\underline{(\gamma_g)_{av} = 0.7507}$$

$$M_g = (\gamma_g)_{av} \cdot M_{air} = 0.7507 \cdot 28.96 = \underline{21.74}$$