



University of  
Stavanger

**FACULTY OF SCIENCE AND TECHNOLOGY**

**DATE: May 5, 2015**

**SUBJECT: PET 565 – Core scale modeling and interpretation**

**TIME: 4 hours**

**AID: No printed or written means allowed. Definite basic calculator allowed.**

**THE EXAM CONSISTS OF 7 PROBLEMS ON 3 PAGES**

**REMARKS: You may answer in English or Norwegian. Exercises 1 - 3 (part A) and exercises 4 - 7 (part B) are given equal weight.**

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**Problem 1.**

- (a) We focus on the model for spontaneous imbibition

$$\phi \partial_t S_w + \partial_x \left( K \frac{\lambda_w \lambda_o}{\lambda_t} \partial_x P_c(S_w) \right) = 0, \quad \lambda_i = \frac{k_{ri}}{\mu_i}, \quad i = w, o \quad (1)$$

where  $\lambda_t = \lambda_w + \lambda_o$  is the total mobility.  $K$  and  $\phi$  are, respectively, absolute permeability and porosity.

- ✓ (i) Formulate the mass balance equations as well as Darcy's law for water and oil.  
 ✓ (ii) Assume countercurrent flow (i.e.,  $u_w = -u_o$ ) and use this to find an expression for  $p_{wx}$  expressed in terms of  $P_{cx}$ , where  $p_w$  is water pressure and  $P_c = p_o - p_w$  is capillary pressure.  
 ✓ (iii) Finally, explain how to obtain (1).

- (b) We introduce the normalized saturation  $S = \frac{S_w - S_{wr}}{1 - S_{wr} - S_{or}}$ , and the dimensionless space variable  $x_D = x/L$ . Use the notation  $P_c(S_w) = \bar{P}_c(S)$ .

(i) Rewrite (1) such that it is expressed in terms of  $x_D$  and  $S$ .

(ii) In the following we skip the "D" index such that  $x = x_D$ . Let  $\bar{S} = \bar{S}(t) = \int_0^1 S(x, t) dx$  and assume that  $S|_{x=0} = 1$  and  $\partial_x S|_{x=1} = 0$ . Derive an equation for  $\bar{S}(t)$ .

- (c) Following the approach discussed in the paper by Tavassoli et al, the following equation can be obtained for  $\bar{S} = \int_0^1 S(x, t) dx$  (after having specified Corey functions, capillary pressure function, dimensionless time, etc.):

$$\frac{d}{dt} \bar{S} = -k_{ro}^{max} J' \varepsilon^b (S_x|_{x=0}), \quad (\varepsilon = 1 - S \text{ as } x \rightarrow 0^+), \quad (2)$$

where  $k_{ro}^{max}$  and  $J'$  are constants related to relative permeability and capillary pressure, respectively, and  $b$  is a Corey exponent. In order to derive an approximate solution it is assumed that  $S(x, t)$  is of the form

$$S(x, t) = \begin{cases} 1 - A(t)x^f, & 0 \leq x \leq x^0; \\ 0, & x^0 \leq x \leq 1. \end{cases} \quad (3)$$

where  $x^0(t) < 1$  represents the foot of the front such that  $S(x^0(t), t) = 0$ . Here  $A(t)$  and  $f$  are unknown and must be determined.

(i) Use (3) and derive an expression for  $\bar{S}(t)$ . Find also an expression for  $x^0(t)$  and use that in combination with the newly found  $\bar{S}(t)$ .

- ✓ (ii) Explain **briefly**, expressed in words, how to proceed in order to find expressions for  $A(t)$  and  $f$ .

- (d) After a series of calculations, it is found that

$$A(t) = \frac{1}{(\beta t)^{f/2}}, \quad \beta = \frac{2(2+b)}{1+b} k_{ro}^{max} J', \quad f = \frac{1}{1+b}$$

(i) Use this information to find an expression for the oil recovery  $\bar{S}(t)$  that reveals how it depends on time  $t$ .

(ii) What is the corresponding expression for the position of the foot of the front  $x^0(t) < 1$ ?

**Problem 2.** The Buckley-Leverett model for injection of water in an oil reservoir takes the form in dimensionless variables

$$\begin{cases} S_t + f(S)_x = 0, & x \in [0, 1] \\ S(x=0, t) = 1, \end{cases} \quad (4)$$

where  $S$  represents the water saturation.

- (a) Give a description (without mathematical derivation) of how to construct the solution after a time  $t > 0$  before the front has reached the producer at  $x = 1$  for a typical choice of the fractional flow function  $f(S)$ .
- (b) Derive (by mathematical calculations) an expression for the oil recovery  $R(t)$  for the solution discussed in (a). Compare this expression for  $R(t)$  with oil recovery for spontaneous imbibition found in (1d) and represented by  $\bar{S}(t)$ . What do these two expressions for oil recovery tell you?

**Problem 3.** Conservation of mass and Darcy's law can be used to derive a conservation law model

$$S_t + g(S)_x = 0, \quad g(S) = -S(1-S), \quad x \in [0, 1], \quad (5)$$

for flow of water ( $S$  is water saturation) and oil ( $1-S$  is oil saturation) in a vertical core plug that is closed at both ends.

- (a) Consider the Riemann problem where the following initial data is assumed

$$S_0(x) = \begin{cases} 1, & x \leq 0.5; \\ 0, & x > 0.5. \end{cases}$$

Compute the solution at time  $T = 0.5$ .

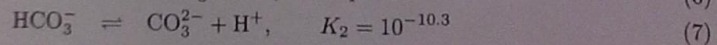
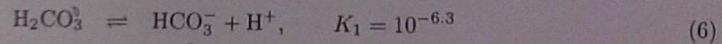
- (b) Consider the Riemann problem where the following initial data is assumed

$$S_0(x) = \begin{cases} 0, & x \leq 0.5; \\ 1, & x > 0.5. \end{cases}$$

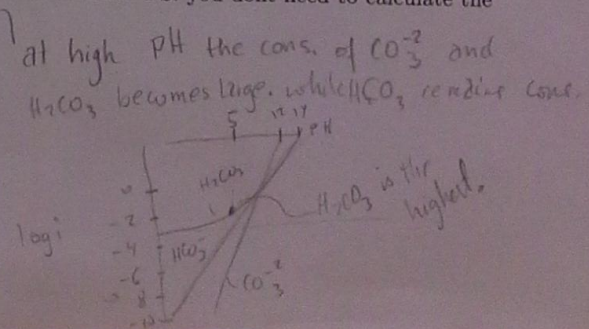
Compute the solution at time  $T = 0.5$ .

- (c) Give a physical interpretation of the solutions obtained in (a) and (b) where it is assumed that  $\rho_w > \rho_o$  (density of water versus oil).

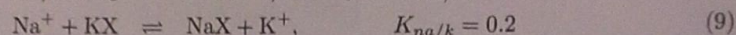
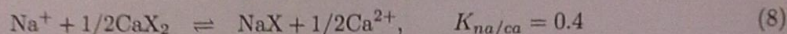
*OK* **Problem 4.** Consider the analysis of a brine sample. The carbon concentration, pH and ionic strength were measured to 0.002 mol/L, 5 and 0.5. Carbon species dissociate according to the following reactions.



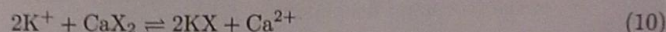
- Write down the equilibrium equations for the two reactions and the mass balance relation between the carbon species concentrations for  $\text{CO}_3^{2-}$ ,  $\text{HCO}_3^-$ ,  $\text{H}_2\text{CO}_3$  and the total carbon concentration.
- Determine activity coefficients for all species involved in the reactions.
- Which carbon species has the highest concentration? PS: you don't need to calculate the individual concentrations.



**Problem 5.** The ions  $\text{Na}^+$ ,  $\text{Ca}^{2+}$  and  $\text{K}^+$  adsorb on a surface which is in equilibrium with a brine of composition  $C_{\text{na}} = 0.05$ ,  $C_{\text{ca}} = 0.02$ ,  $C_{\text{k}} = 0.03$ . Exchange reactions are given as follows:



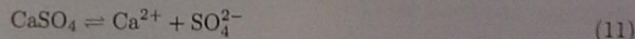
- Write down equilibrium and mass balance equations for the system.
- Calculate the composition on the rock surface in terms of equivalent fractions.
- Define and calculate the equilibrium constant for the exchange reaction



**Problem 6.** A species adsorbs according to  $q = 0.5c^2$  where  $c$  is concentration and  $q$  (mmol/L pore) is the adsorption isotherm (amount adsorbed species as function of brine concentration). A 0.1m sample contains 2mmol/L formation water and we flood with a brine containing 3mmol/L. The cross-sectional area is 0.0005 m<sup>2</sup> and the porosity of the sample is 0.2.

- At the time the water front has reached the core end, 0.1m, sketch the concentration profile  $c(x)$ .
- How many moles are retained from the injected fluid by adsorption after flooding (at a time when the injected concentration is obtained at the outlet)?

**Problem 7.** A rock sample contains amounts of the salt anhydrite  $\text{CaSO}_4$ . The core is flooded with distilled water. The salt dissolves according to the reaction



- Suggest a rate expression for the dissolution reaction based on the saturation state of  $\text{CaSO}_4$ .
- Write a transport model for the ions  $\text{Ca}^{2+}$ ,  $\text{SO}_4^{2-}$  and the salt  $\text{CaSO}_4$ . Include dispersion, advection and dissolution.
- Sketch the expected time profile of the effluent of the ions  $\text{Ca}^{2+}$ ,  $\text{SO}_4^{2-}$ . List your assumptions.
- Would it make a difference for the process to flood the core with NaCl instead of distilled water? Discuss.

#### APPENDIX A. FORMULAS

Davies formula (at 25°C):

$$\log_{10} \gamma_i = -0.5085 Z_i^2 \left( \frac{\sqrt{I}}{1 + \sqrt{I}} - 0.3I \right) \quad (12)$$

Retardation formula

$$R_c = 1 + \frac{dq}{dc}, \quad (\text{broadening front}) \quad (13)$$

$$R_f = 1 + \frac{\Delta q}{\Delta c}, \quad (\text{sharpening front}) \quad (14)$$

pH

$$\text{pH} = -\log_{10}([\text{H}^+]) \quad (15)$$